

SELECTIVITY IN HETEROGENEOUS CATALYTIC OXIDATION

Jerzy HABER

Research Laboratories of Catalysis and Surface Chemistry,
Polish Academy of Sciences, Kraków, Poland

Abstract - Selectivity of the catalytic oxidation of hydrocarbons is discussed in terms of the type of intermediate complex formed. Two different intermediate complexes initiate two different routes of the reaction. Activation of oxygen leads to total oxidation through electrophilic attack on the double bond and formation of the complex of the peroxide or epoxide type, whereas partial oxidation requires activation of the hydrocarbon molecule resulting in the formation of the allyl species bonded as ligand in the intermediate complex. It proceeds then in a series of consecutive oxidative elementary steps, each of them requiring different active centers to be present at the catalyst surface. The type of product obtained and its selectivity depend thus on the type and mutual proportions of these centers. Oxidation is performed by the cationic active centers, whereas oxygen is inserted by a nucleophilic attack which may also be considered as an acid-base process. Mechanisms of these elementary steps are discussed on the basis of the quantum chemical description of intermediate complexes.

Reactions of the catalytic oxidation of hydrocarbons have been studied extensively in the past decade/1-4/ because of their great importance for the development of chemical industry. The introduction of bismuth molybdate as catalyst for the selective oxidation of propylene to acrolein by Vestch and Callahan /5/ and the development of the synthesis of acrylonitrile by ammoxidation of propylene on this catalyst may be considered as turning points in the history of modern petrochemistry /6/. However, also some of the older catalytic processes such as oxidation of naphthalene and o-xylene to phthalic anhydride found considerable interest because of the fact that although they have been operated in industry for many decades, their mechanism is not yet understood. On the other hand catalytic oxidation of hydrocarbons is very interesting from the theoretical point of view, as the organic molecule can in most cases react at the surface along several different reaction paths, giving several different products. Often small modification of catalyst composition or variation in the method of its preparation can modify its catalytic properties to such an extent, that the direction of the reaction is changed and a new product is formed, usually with high selectivity. This creates particularly favourable conditions for

studying the correlation between properties of the catalyst and the selectivity of its catalytic performance, which enables important conclusions to be drawn, concerning the theoretical basis for the selection of catalysts.

Selectivity of catalytic reactions may be discussed in terms of the type of intermediate complex formed at the surface of the catalyst in the course of the reaction. Three limiting cases may be distinguished as shown in Fig.1:

- a/ from a given substrate the same intermediate complex is always formed, but depending on the catalyst the potential barrier along different reaction coordinates is lowered and different products are thus formed;
- b/ depending on the catalyst different intermediate complexes are formed, which then transform into different products;
- c/ in a series of consecutive steps several intermediate complexes are formed which either desorb to give one of the intermediate products, or transform consecutively into each other.

Ample experimental evidence indicates that highly reactive adsorbed oxygen radicals are responsible for the reactions of the total oxidation of hydrocarbons. Results of the study of oxygen isotope exchange and of tracer experiments with oxygen isotopes are particularly relevant. Comparison of numerous data on the rate of homomolecular exchange of oxygen on various transition metal oxides, determined by Boreskov and his school /7,8/ with the data on catalytic activity of these oxides in the total oxidation of several simple compounds revealed a close correlation between the ability of the oxide to activate oxygen and its activity in the catalytic reaction.

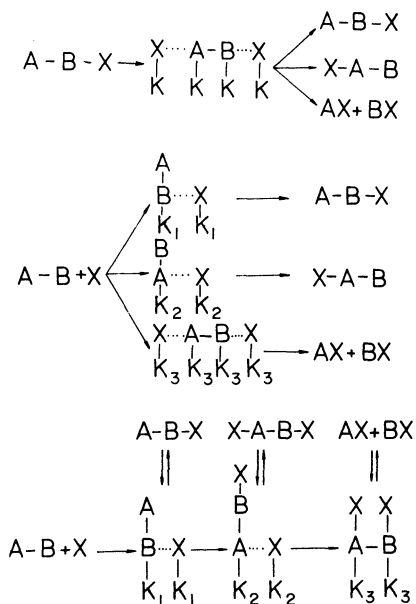
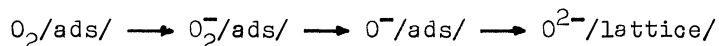


Fig.1. Role of intermediate complex in determining the selectivity of the catalytic reaction.

On the other hand Keulks et al /9/ have shown that when propylene is oxidized in oxygen containing ^{18}O , this isotope does not at the beginning of the reaction appear in acrolein. This indicates that lattice oxygen and not the adsorbed one is involved in selective oxidation. Classical experiments described by Sachtler /1,10/, in which oxidation over oxide catalysts was carried out with propylene labelled by ^{14}C in the α -carbon position, have shown that in the resulting acrolein ^{14}C is evenly distributed between both terminal carbons. This was taken as a proof that in the first step of the reaction propylene is activated by abstraction of α -hydrogen and formation of an allylic species.

Thus the general conclusion may be formulated that two different intermediate complexes /case b/ initiate two different paths of the reaction of catalytic oxidation of hydrocarbons, one leading to partial oxidation products and the second resulting in total oxidation. Partial oxidation requires activation of the olefin molecule, resulting in the formation of the allyl species bonded as a ligand in the intermediate complex, but no activation of oxygen should take place. The catalyst to be selective in allylic oxidation should not contain at the surface any adsorbed oxygen. Heterogeneous activation of oxygen leads to total oxidation. Oxygen, adsorbed in form of O_2^- or O^- species is a strongly electrophilic reagent which attacks the organic molecule in the region of its highest electron density, i.e. at the double bond in the case of olefin, forming an intermediate complex of the peroxide or epoxide type.

Many observations indicate /11,12/ that adsorbed oxygen species transform at the surface of an oxide according to the general scheme:



in which they are gradually enriched with electrons.

Depending on the properties of the solid and the experimental conditions certain transformations may be faster or slower and usually only one form is predominant in the steady-state. From this point of view all the oxide catalysts may be divided into three groups /13/. The first group comprises oxides characterized by high concentration of centers which can supply electrons to the adsorbed oxygen molecules. These are oxides showing p-type semiconductivity, as this property is related to the presence of transition metal cation of low ionisation potential. At their surface oxygen is adsorbed predominantly in the form of electron rich species. Second group of oxides is characterized by a low concentration of electron donor centers. These are n-type semiconducting oxides, diluted solid solutions of transition metal ions in diamagnetic matrices or transition metal oxides highly dispersed on carriers. They adsorb oxygen in the form of species less rich in electrons. Third group is formed by mixed oxides of the oxysalt type in which oxygen atoms are present in form of well defined oxyanions with the transition metal ion at its highest oxidation state as the central atom. Studies of the adsorption of oxygen on different series of transition metal oxysalts showed /14,15/ that it rapidly decreases with increasing ionisation potential of the transition metal cation and increasing covalency of bonds in the anionic group. This may be interpreted in terms of decreasing electron donor properties of transition metal ions at the surface

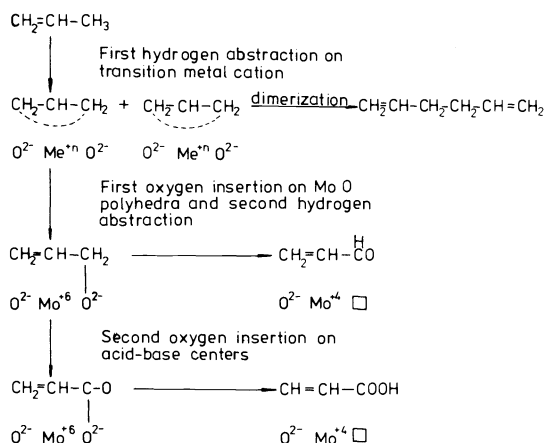


Fig.2. Mechanism of the selective oxidation of olefins.

of the solid with decreasing ligand fields of oxygen ions due to the change of polarisation of bonds within anionic group.

Reaction path leading to partial oxidation, may be considered as a series of consecutive oxidative steps, each of them consisting in one elementary transformation of the reacting molecule and formation of a different intermediate complex /case c/. Some years ago we have advanced a multicenter model of such processes /16,17/. Main features of this model are /Fig.2/:

- activation of the olefin molecule, consisting in the abstraction of α -hydrogen and formation of π -bonded allylic species, takes place on cationic active centers. In the case of molybdates, tungstates etc. these centers involve oxygen polyhedra of such cations as Bi^{+3} , Co^{+2} , Ni^{+2} etc.;
- when no other centers are present at the surface, the π -allyl species recombine to give dimers of diene type or form polyenes by repetition of the first step on cationic active centers;
- different active centers at catalyst surface are required for the insertion of oxygen. Oxygen polyhedra of molybdenum, tungsten etc. are involved in creation of these centers, on which the allylic species transform into allyl species σ -bonded to lattice oxygen ions of these. They may desorb in the form of aldehyde leaving an oxygen vacancy on the surface of the catalyst,
- third type of active centers is involved in the insertion of a second oxygen atom into the organic molecule, resulting in the formation of a carboxylate intermediate complex, which then desorbs in the form of acid.

In order to study in more detail the role of the metal cations in the first step of the reaction a series of isostructural compounds: $\alpha\text{-CoMoO}_4$, NiMoO_4 , MnMoO_4 and MgMoO_4 was investigated in the oxidation of propylene to acrolein /18/. Results of the pulse reactor measurements are summarized in Table 1. As seen from this table, $\alpha\text{-CoMoO}_4$ and MnMoO_4 show considerable selectivity in the formation of acrolein, whereas MgMoO_4 is completely inactive. The sublattice of Mo-O polyhedra being identical, this

TABLE 1. The activity of the isostructural molybdates CoMoO_4 , MnMoO_4 and MgMoO_4 and the related oxides in their interaction with propylene^{x/} /18/

Catalyst	Temp. (°C)	Conversion of C_3H_6 /%/	Selectivity /%/			Other products
			$\text{C}_2\text{H}_6\text{O}$	C_6H_6	CO_2	
-CoMoO_4	490	95	30	10	50	cracking
MnMoO_4	490	30	36	-	39	cracking
MgMoO_4	490	10	-	-	100	
CoO	450	95	-	30	20	cracking
MgO	490	4	-	-	100	

^{x/} Pulse method: 1 pulse = 10.2×10^{-6} mol C_3H_6

difference must be due to differences in the properties of cationic active centers. To find which properties of the cation are relevant to the ability to activate the olefin molecule, quantum chemical calculations have been carried out /19/ of the charge distribution, electronic configuration and orbital energy of hypothetical first intermediate surface complexes of metal cations assumed to be octahedrally coordinated by five identical oxygen ligands, the sixth ligand being the allyl radical. Some of the results of the calculations by the SCCO MO method are shown in Table 2. In the case of Co^{+2} and Ni^{+2} complexes there is a considerable shift of π -allyl electrons to the metal, the positive charge appearing thus on the allyl ligand, whereas in Mg^{+2} complexes the allyl remains neutral indicating a very weak binding. Comparison of these data with the catalytic activity of Co, Ni and Mg molybdates /cf. Table 1/ leads to the conclusion that ability of the cation

TABLE 2. Results of theoretical calculations /19/

Metal	Number of un- paired elec- trons in the complex ion	Average number of π - elec- trons on allyl	Populations in allyl orbitals			Charge on carbon atoms /in e units/			
			π_1^b	π_2^n	π_3^a	Terminal		Central	
						π -Elec- tronic contri- bution	Total charge	π -Elec- tronic contri- bution	Total charge
-	1	3	2	1	0	-0.025	-0.096	0.050	0.057
Co^{2+}	4	2.426	1.301	1.039	0.086	0.119	0.048	0.347	0.354
Co^{2+}	0	1.478	1.429	0.027	0.021	0.606	0.535	0.310	0.317
Ni^{2+}	3	2.318	1.284	1.021	0.013	0.149	0.078	0.383	0.390
Ni^{2+}	1	1.365	1.286	0.068	0.011	0.625	0.554	0.383	0.390
Mg^{2+}	1	2.849	1.800	1.033	0.016	0.007	-0.064	0.136	0.143
Mo^{6+}	1	0.836	0.768	0.053	0.015	0.768	0.697	0.627	0.634
Mo^{5+}	2	1.039	0.901	0.123	0.015	0.699	0.628	0.564	0.571
Mo^{5+}	0	0.905	0.828	0.053	0.023	0.750	0.769	0.594	0.601
Mo^{4+}	3	1.046	0.903	0.123	0.020	0.687	0.616	0.561	0.568
Mo^{4+}	1	1.203	0.962	0.228	0.013	0.633	0.562	0.536	0.544

to bind π -allyl is a condition necessary for its role as the active center of the first step of the reaction.

As in the majority of the partial oxidation reactions the first step is rate determining, studies of these reactions cannot yield any information on the next stages of the reaction. One of the ways by which the discussed model could be confirmed and the mechanism of the insertion of oxygen studied in more detail, is to by-pass the first step by generating the allyl radicals by some other more effective route. This was effected /20/ by using allyl iodide, which readily decomposes into allyl radicals. The first step of the selective oxidation is thus facilitated, making possible the examination of the conditions which are necessary for the insertion of oxygen in the next step of the reaction.

Important conclusions may be drawn from the comparison of the behaviour of Bi_2O_3 and MoO_3 in the reactions with propylene and allyl iodide /Table 3/. When allyl iodide is passed over MoO_3 , already at 310°C practically total conversion is observed with 98 % selectivity to acrolein. In the same conditions MoO_3 is completely inactive with respect to propylene. On contacting allyl iodide with Bi_2O_3 , total conversion at 310° was also observed. In this case however 70 % of the products formed was 1,5-hexadiene, practically no acrolein being detected. Comparison with the results for homogeneous reaction indicates that hexadiene was formed mainly as the result of heterogeneous reaction at the surface of Bi_2O_3 , because at 310° only about 20 % conversion is observed in homogeneous reaction. 1,5-Hexadiene as the product was also obtained in the reaction of propylene on Bi_2O_3 . These results confirm the validity of the multicenter model of molybdate catalysts, which we have advanced. As the role of Bi-centers in selective oxidation catalysts consists in generation of allyl species, change of the reactant from propylene to allyl radicals formed in situ in the reactor as the result of the decomposition of allyl iodide does not change the reaction pattern, only higher yield of 1,5-hexadiene is observed. Different situation exists in the case of MoO_3 . Its surface contains active centers which are able to

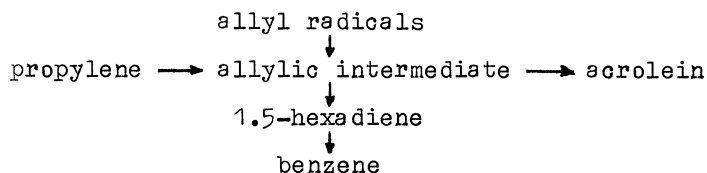
TABLE 3. Interaction of propylene and allyl iodide with molybdates /20/

Catalyst	PROPYLENE			ALLYL IODIDE					
	Temp. $^\circ\text{C}$	Yield, %			Temp. $^\circ\text{C}$	Yield, %			
		Hexa- diene	Ben- zene	Acro- lein		Propy- lene	Hexa- diene	Ben- zene	Acro- lein
Bi_2O_3	480	8.6	-	-	310	- (2.0)	70.0 (8.0)	- (-)	5.0 (-)
MoO_3	480	-	-	-	310	-	-	-	98.0 (-)
Bi_2MoO_6	460	-	-	13.0	310	-	12.0	3.0	15.0
$\text{Mg}_2\text{Mo}_3\text{O}_{11}$	480	-	-	1.0	370	15.0 (25.0)	10.0 (25.0)	- (2.0)	25.0 (-)
MgMoO_4	480	-	-	-	-	61.0 (62.0)	0.7 (7.0)	1.3 (7.0)	- (-)

Numbers in brackets - homogeneous reaction

perform the insertion of oxygen into the organic molecule. However MoO_3 is inactive in propylene oxidation because no centers are available for efficient generation of allylic species. When, however, such species are formed by some other route, their total conversion to acrolein at MoO_3 surface takes place.

An efficient catalyst for the oxidation of propylene to acrolein is therefore characterised by two functions: activation of propylene by formation and bonding of allylic species, and insertion of oxygen into the hydrocarbon molecule. In complex oxide catalysts these functions are played by different lattice constituents as Bi-O and Mo-O polyhedra. However, it may also be visualised that a single oxide has both kinds of centers present at the surface. The overall reaction may be described by a series of of consecutive, parallel steps:

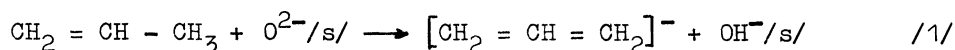


Even when both kinds of active centers are present at the surface of the catalyst as it is the case in Bi_2MoO_6 , the acrolein/diene ratio will depend on the ratio of the rate constants. In the case of the oxidation of propylene, its adsorption (which is equivalent to its activation to allylic intermediate) is rate determining /21/. In such conditions the surface of the catalyst is scarcely populated with allylic intermediates, which immediately react to acrolein, the selectivity of this product thus being very high. When however the surface is contacted with allyl radicals generated in the gas phase by decomposition of allyl iodide, the coverage of the surface with adsorbed allylic intermediate may attain much higher values and the probability increases that two such species will be adsorbed at adjacent centers and recombine to form 1,5-hexadiene. Table 3 shows that in fact the reaction of the allyl iodide at the surface of Bi_2MoO_6 results in the formation of certain amount of 1,5-hexadiene and benzene and consequently much lower selectivity to acrolein than that observed in oxidation of propylene. When active centers for oxygen insertion are removed by replacing molybdate anions with e.g. phosphate, the reaction path to acrolein is eliminated and high conversion to benzene is observed /22/.

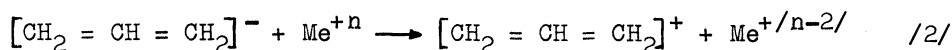
Some time ago Seiyama et al /23/, Golodets /24/ and Ai /25/ advanced a hypothesis that different behaviour of oxides in the oxidation of hydrocarbons may be related to their acid-base properties. Although this parameter is certainly of great importance, it is only one of the factors influencing some of the elementary steps and should be discussed only in relation to these steps.

Activation of the olefin molecule in the first step of the reaction, consisting in the abstraction of α -hydrogen, may proceed either as a homolytic or heterolytic bond rupture. Although the homolytic rupture of C-H bond in homogeneous reaction is energetically more favourable than the heterolytic one, the latter may be rendered much easier by interaction with the surface of an oxide of acid-base properties. In the presence of lattice

oxygen ions of basic character the first step of the oxidation of e.g. propylene could be written as

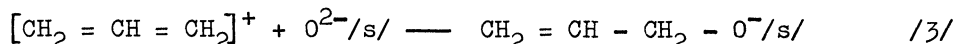


which may be considered as an acid-base reaction. As however shown by quantum-chemical calculations /19/ discussed above, the electron transfer from the adsorbed allyl to the metal cation of the catalyst lattice rendering the allyl species positive must take place before this species can react further with the lattice oxygen. A second process must thus occur, which can be described by the equation:



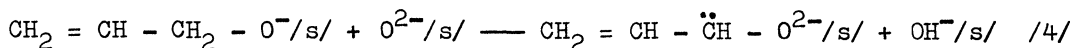
This is a pure redox process. The catalyst, in order to activate the hydrocarbon molecule for further oxidative transformation, must thus be able to perform both functions. It is obvious that the two stages may proceed as one concerted reaction of mixed redox acid-base character. When comparing samples of the same catalytic system, characterized by a given redox potential, but differing in acid-base properties due to appropriate additions, a correlation may be observed between the catalytic activity and acidity as described by Ai /26/ for the case of $\text{Bi}_2\text{O}_3\text{-MoO}_3\text{-P}_2\text{O}_5$ system of different P_2O_5 content. On the other hand, in comparing different catalytic systems, the differences in their redox properties may well be of much greater significance than those in acid-base character.

The second step in the selective oxidation consists in the nucleophilic addition of lattice oxygen ion to the allyl species:

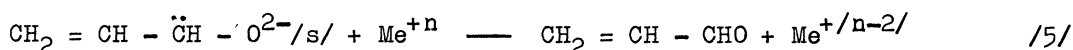


In terms of the Guttmann definition it is an acid-base process with O^{2-} transfer. As, however, insertion of oxygen is performed by very few oxides (although many others are known of similar acidity) it seems more plausible to assume that some other properties of the oxide lattice beside the basicity of the oxide ions must be responsible for its ability to insert oxygen into an organic molecule.

Decomposition of the surface complex with desorption of acrolein may also be considered to proceed in two states, of which one is of acid-base character:



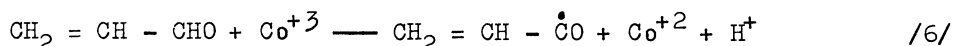
and the second of redox character:



Let us now pass to the discussion of the mechanism of the third step of partial oxidation, consisting in the oxidation of the aldehyde to the acid. Comparison of the literature and patent data shows that on some catalysts such as bismuth molybdate or tin antimonate only acrolein is formed as the result of the oxidation of propylene, whereas with other catalysts, e.g. cobalt and nickel molybdate, acrolein and acrylic acid are obtained in different proportions depending on the conditions of the experiment. The ability to transform the aldehyde into an acid seems to be a more general property as indicated by the data of Table 4, in which results /27/ are summarized concerning the selectivity of the same catalysts in the oxidation

of o-xylene. On catalysts, which oxidize propylene only to acrolein, o-xylene is oxidized only to toluylaldehyde, whereas phthalic anhydride is formed only with those catalysts, on which acrylic acid appears as the result of the oxidation of propylene. Thus, it may be concluded that a special type of active center must be present at the surface of the catalyst, which has the ability to transform the aldehyde group into the carboxylic group irrespective of the type of the organic molecule.

It is well known that cobalt compounds are very effective catalysts in both homogeneous and heterogeneous oxidation of aldehydes to acids. In homogeneous reactions complexes of Co^{+3} ions with oxygenated organic ligands are used as catalysts, in which Co-ion is surrounded by an octahedron of oxygen atoms. It has been postulated /28/ that the role of Co^{+3} complex consists in the generation of radicals according to the equation:



These radicals then react with oxygen to give the superacid radicals, which transform into superacid molecules. Acceleration of their decomposition is the second function of Co-complexes.

In the heterogeneous oxidation of acrolein, carried out at much higher temperatures, cobalt molybdate has been found to be active and selective catalyst. Similarly as homogeneous catalysts they contain cobalt ions directly linked to oxygen ions in an octahedral arrangement.

Many experimental data seem to indicate, that in the step acrolein — acrylic acid on cobalt molybdate catalysts it is the surface cobalt ion which

TABLE 4. Oxidation of o-xylene on olefin oxidation catalysts /27/

Catalyst	Temp. °C	Conv. %	Selectivity, %		
			tolualdehyde	phthalic anh.	CO ₂
Bi ₂ Mo ₂ O ₉	370	5.5	45.4	-	52.8
	430	35.0	33.7	-	54.3
	470	49.5	29.9	-	52.9
Bi ₂ MoO ₆	370	18.5	45.4	-	45.9
	430	52.5	34.7	-	54.5
	470	71.7	25.6	tr.	58.0
Sn-Sb-O (Sn/Sb=1/4)	390	7.5	45.3	-	49.3
	450	21.0	34.0	-	54.8
	490	42.0	24.0	-	70.2
CoMoO ₄	390	30.0	12.0	10.6	60.0
	410	56.0	5.2	26.4	57.0
	450	94.0	tr.	36.4	48.0
	470	98.0	tr.	31.2	48.0
NiMoO ₄	370	40.0	6.8	13.0	62.8
	390	76.0	2.5	19.5	71.0
	410	93.0	1.0	29.0	62.4
	450	99.0	tr.	25.2	56.0
MoO ₃	450	15.0	50.0	3.3	32.7
	490	30.5	51.1	2.3	30.8
V ₂ O ₅ -TiO ₂ (V/Ti=1/2)	350	29.0	14.5	34.8	32.4
	370	65.0	7.1	49.2	21.4
	390	99.0	-	64.5	27.6

is involved as active center. The molecular mechanism of the catalytic action of cobalt ions, linked to oxygens in octahedral coordination must thus account for the possibility of both processes, depending on the properties of the coordination sphere of cobalt ions /isolated complex or complex constituting an element of crystal lattice/ as well as on conditions of experiment /temperature and the presence of solvent molecules/.

The information on the type of bonding of acrolein in the intermediate complex may be obtained from the infrared spectra of acrolein adsorbed at the surface of the cobalt molybdate catalyst adsorbed on MgO with a large surface /fig.3/ /29/. Appearance of the new absorption bands at 1660 cm^{-1} and 1310 cm^{-1} after heating at 200°C indicates that the aldehyde group has been bonded to a surface oxygen ion forming the carboxylate anion. The presence of the band at 1500 cm^{-1} may be interpreted as due to a considerable weakening of the double bond, hinting to its interaction with the surface metal ions. A model of the surface intermediate complex may thus be formulated /30/, in which acrolein as the sixth ligand is coordinated to the surface cobalt ion by the double bond, the aldehyde group interacting with the surface oxygen ion forming the octahedral surrounding of the cation /fig.4/. This model was taken as the basis for quantum-chemical calculations of the electron distribution and energy, carried out by the semiempirical SINDO method. Analysis of the results of calculations led to the conclusion /30/ that a strong interaction exists between hydrogen atom of the aldehyde group and nearest oxygen atom of the complex, resulting in considerable weakening of the C-H bond. A transformation may thus occur consisting in the transfer of proton to oxygen with the heterolytic rupture of C-H bond, accompanied by a rearrangement of electrons resulting in the homolytic rupture of bond between the vinyl group and Co-ion. Such transformation is equivalent to reaction /6/ postulated to be the initiation of the catalytic homogeneous oxidation.

Results indicate that there is a strong interaction of the planar oxygen of the complex not only with hydrogen but also with carbon of the

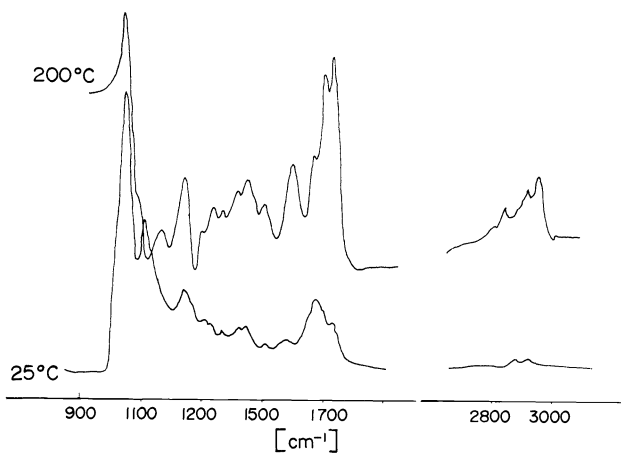


Fig.3. Infrared spectra of acrolein adsorbed on $\text{CoMoO}_4/\text{MgO}$ catalyst at 20°C and 200°C . /29/

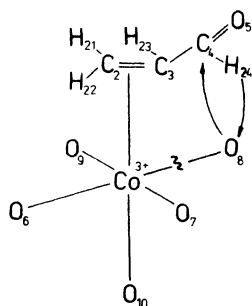


Fig.4. Concerted mechanism of the oxidation of acrolein to acrylic acid on cobalt complex. /30/

aldehyde group, resulting in simultaneous weakening of the Co-O bond, as indicated in Fig. 4. At elevated temperature of the heterogeneous process a concerted reaction may now occur, consisting in the transfer of proton from carbon to oxygen, formation of the bond between oxygen and carbon and rupture of Co-O bond, provided lattice oxygen of the catalyst is enough mobile. This may be the case in the molybdate structures in which easy transformation of the lattice from corner-linked octahedra into an edge-linked arrangement makes abstraction of oxygen very facile. Such concerted reaction may be considered as equivalent to the insertion of oxygen into the C-H bond of the aldehyde group.

The existence of different active centers, at which the gives series of consecutive elementary steps may proceed resulting in the formation of a given product is the condition necessary but not sufficient for a catalyst to be effective. The product must be also readily desorbed from the surface.

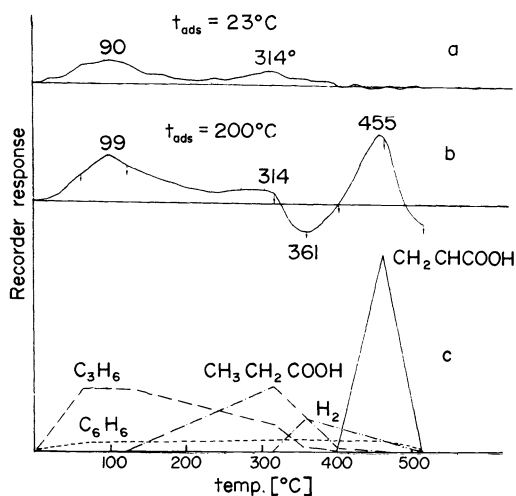
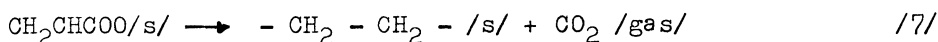


Fig.5. Thermoprogrammed desorption from the surface of CoMoO_4 after preadsorption of propylene /31/ at: a/ 25°C , b/ 200°C , c/ results of the analysis of products desorbed at 200°C .

In the oxidation of propylene to acrolein this is the case with such catalysts as bismuth molybdate or MoO_3 , which in the conditions of the catalytic reaction practically do not adsorb acrolein. In the case of pure stoichiometric cobalt molybdate, acrolein is adsorbed irreversibly /31/. Thermodesorption experiments indicate /31/ that after contacting cobalt molybdate with propylene at 250°C , no acrolein can be detected in the products of desorption, but above 400°C acrylic acid comes off from the surface /fig.5/. This indicates that at the surface of cobalt molybdate propylene is easily oxidized to acrolein but the desorption rate of acrolein as the intermediate product is (in the conditions of thermodesorption experiment) negligible in comparison with the rate of its transformation into the carboxylate-like complex by interaction with the next lattice oxygen ion. This complex decomposes with the desorption of acid only when the surface is fully oxidized. As soon however as it becomes reduced in the conditions of the reaction, the strength of bonding of the complex with the surface increases, as manifested by considerable increase of adsorption of acrolein on reduction /31/. Decarboxylation of the surface complex takes then place, resulting in the deposition of coke according to the reaction



Taking into account that oxygen atoms in the carboxylate complex are surface oxygens of the molybdate lattice, decarboxylation of this complex results in the formation of oxygen vacancies, equivalent to the reduction of the solid and deposition of the organic residue. The ratio of the rate of reduction of the solid with propylene, v_r , to the rate of coke deposition, v_c , should thus be constant irrespective of the conditions of experiment. This is indeed the case as shown by the results of the measurements of reduction of cobalt molybdate in propylene and acrolein /32/ summarized in Table 5.

The mechanism of the decarboxylation of carboxylate complexes at the surface of CoMoO_4 was confirmed by the electron spectroscopy /33/. As an example, fig.6. shows the spectra recorded in the course of transformations of acrolein at the surface of CoMoO_4 .

Table 5. Carbonization of the CoMoO_4 samples in the course of the reduction /32/

Reducing gas	Temperature $^\circ\text{C}$	Degree of reduction %	Oxygen consumption $\text{mol} \cdot 10^4$	Amount of CO_2 formed $\text{mol} \cdot 10^4$	H : C	v_c/v_r
Propene	470	37.5	2.88	1.37	1.86	0.68
	500	16.6	1.35	0.79	0.6	0.71
		48.0	3.58	1.58	2.3	0.66
		64.0	5.03	1.57	2.2	0.63
		91.5	5.85	2.06	2.3	0.85
530	39.7	2.58	1.20	1.88	0.65	
Acrolein	500	20-80	-	-	-	0.71
Propion-aldehyde	500	15-65	-	-	-	0.43

Spectrum 1 of initial sample shows the Mo3d doublet at 235.4 and 238.4 eV, and the O1s peak at 533.2 eV. Small carbon residue shows up in form of the C1s signal at 287.6 eV. After adsorption of acrolein at liquid nitrogen temperature /Spectrum 2/ the Mo3d and O1s peaks of the solid disappeared indicating total coverage of the surface with the adsorbed layer thick enough to give a spectrum, which could be considered as characteristic of the adsorbate. It reveals the presence of two C1s peaks at 285.1 and 288.0 eV, their intensity ratio being approximately 2:1. They may thus be interpreted as related to the two different carbon atoms in acrolein. The effective charge on carbon atom in aldehyde group is more positive than the charge of atoms of the vinyl group, and the B.E. value of C1s electrons is higher. The position of carbonyl oxygen amounts to 532.8 eV. On heating to room temperature carbonyl carbon peak disappears, whereas that of vinyl group shifts to 286.8 eV and its intensity considerably increases /Spectrum 3/. Simultaneously the O1s peak shifts at first to 534.3 eV and then starts to decrease in intensity as lattice O1s peak at 532.6 eV reappears indicating that the transformations of species in the chemisorbed layer are now being observed. Apparently two processes have taken place in the course of heating. The vinyl carbon peak shifted to higher B.E. and assumed the value similar to that of C1s electrons of paraffinic chain carbons, observed after adsorption of propionic acid. This may be explained by assuming that polymerisation of acrolein took place and the vinyl carbons disappeared as the result of the formation of paraffinic chains. A second process must be responsible for the shift of the B.E. of oxygen to higher value, close to that of oxygen in adsorbed carboxyl group, in which oxygen atom has a more positive effective charge. We may thus assume that the aldehyde group of acrolein has reacted with the lattice surface oxygen ion forming the chemisorbed carboxyl group.

After outgassing the sample for two hours at 593°K the O1s peak at 534.3 eV related to carboxyl groups disappeared completely /Spectrum 4/,

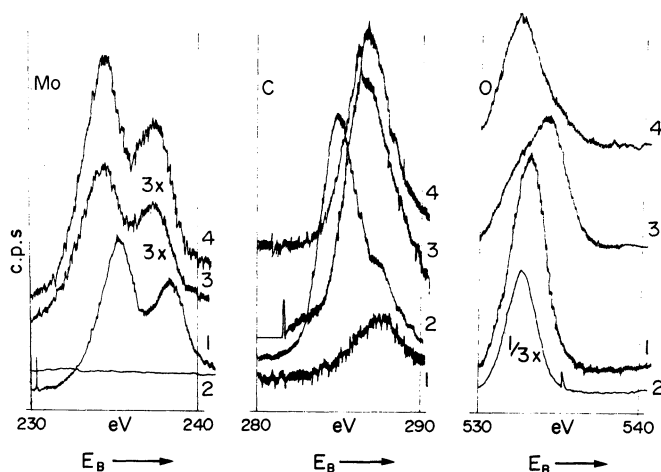


Fig.6. ESCA spectra of Mo3d, C1s and O1s electrons in the course of transformations of acrolein on CoMoO_4 , 1 - initial sample, 2 - after adsorption at 77°K, 3 - after desorption at 298°K, 4 - after outgassing at 593°K for 1.5 hr. /33/

whereas the intensity of C1s peak practically did not decrease. This indicates that decarboxylation of the oxygenated hydrocarbon species took place on heating, leaving at the surface a deposit of polymerised chains. The spectrum remained unchanged after contacting the sample with 0.1 Tr of oxygen for 0.5 hr at 523^oK, however, in comparison with the initial sample, the intensity of Mo3d, Co2p and lattice O1s peaks was about 50 % lower confirming the presence of strongly chemisorbed species.

When discussing the properties of an active catalyst it should be borne in mind that all functions mentioned until now as requirement for selective oxidation are necessary but not sufficient.

After the given elementary step of the catalytic reaction has taken place with the participation of lattice oxygen and formation of oxygen vacancy the active center at the surface is left in the reduced state. Before such elementary step can be repeated, the active center must be reoxidised. This reoxidation can be realised in three ways, as shown in Fig. 7: by incorporation of oxygen from the gas phase /I/, by diffusion of oxygen ions from the bulk /II/ and by the diffusion of the reduced lattice constituents to the nuclei of the new phase of reduced solid and exposition of the underlying fresh crystal planes /III/. Depending on the rate of such regeneration of the active center, its "dead time" may be shorter or longer. In the case of such lattices as bismuth molybdate the mobility of lattice oxygen is very high and process /II/ operates very effectively. In such conditions the "dead time" of active centers is very short, the turn-over number on these centers is very large and the catalyst shows high activity. This process of regeneration does not however operate in cobalt molybdate. When oxygen is present in the gas phase, regeneration of active centers takes place by path /I/ whereas in the absence of gaseous oxygen only path /III/ remains for regeneration. As however the rate of nucleation of reduced phases, which in this case are cobalt molybdite and cobalt-molybdenum /IV/ - spinel /34/ ; and of their growth is very low at the temperature of the catalytic reaction, the activity of the cobalt molybdate drops in the absence of gaseous oxygen to a very low value.

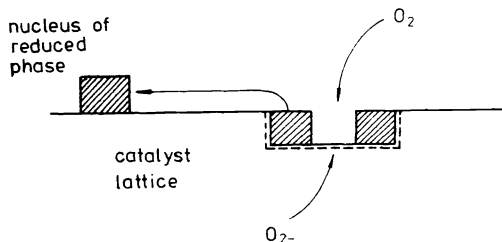


Fig.7. Mechanism of the regeneration of an active center at the surface of oxide catalysts. I - by reoxidation with gaseous oxygen, II - by diffusion of lattice oxygen ions, III - by nucleation of the reduced phase and exposition of a new lattice plane.

The question may now be raised as to which parameters of the solid are responsible for the very high mobility of oxygen in bismuth molybdate as opposed to cobalt or nickel molybdate. Studies of the mechanism of the reduction of group VIb transition metal oxides have led in recent years to the discovery of the phenomenon of crystallographic shear. Removal of oxygen ions from the lattice of these oxides results in the formation of ordered arrays of oxygen vacancies, followed by a very facile rearrangement of the layers of initially corner-linked metal-oxygen octahedra into an arrangement of edge-linked octahedra, resulting in the formation of a shear plane. This is shown in Fig.8. It was recently suggested /35/ that this process may be responsible for a very rapid transport of oxygen observed in lattices of such oxides as compared with the diffusion of oxygen in closepacked structures of the majority of transition metal oxides. On the other hand we would like to point out that the easy evolution of one oxygen ion in the transformation from corner-linked to edge-linked arrangement of M_O-O octahedra may be one of the factors creating the ability of these structures to insert oxygen into the organic molecule in processes of selective oxidation of hydrocarbons.

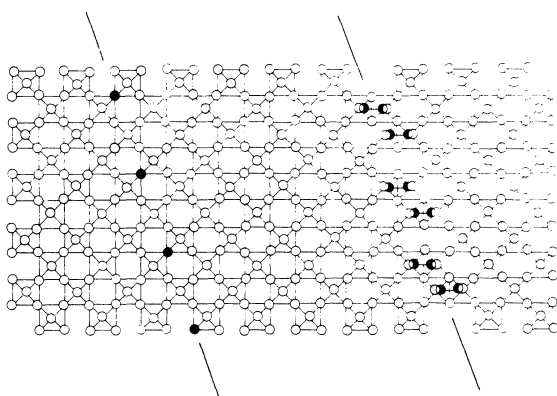


Fig.8. Formation of a shear plane in WO_3 structure.

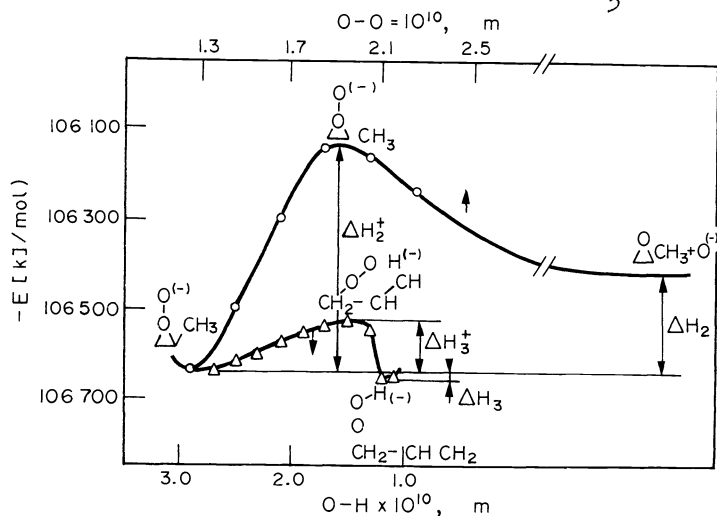


Fig.9. Total MINDO/2 energies plotted against the O-O distance and the O-H distance. /40/

Interesting informations on the changes of the bond structure accompanying the formation of shear planes in various stages of the reduction of group VA, VIA and VIIA metal oxides and its bearing upon the mechanism of the reduction of their more complex compounds as oxysalts were quite recently obtained by photoelectron spectroscopy /36,37,38/.

When discussing the selectivity of catalytic reactions it should always be borne in mind that even when the same intermediate complex is formed at the same active center of the catalyst surface, different reaction paths may be followed depending on the structure of the reacting molecule. Introduction of a new functional group into the organic molecule may namely influence, by the inductive or mesomeric effect, the reactivity of the intermediate complex to such an extent that the mechanism of its transformation is completely changed. Oxidation of ethylene to ethylene oxide on silver catalysts may serve as an example. As shown by Sachtler et al /39/ the role of silver consists in the activation of the oxygen molecule into a superoxide ion O_2^- , which then reacts with ethylene to form ethylene oxide with simultaneous splitting of the O-O bond. Recently Zahradnik et al /40/, using the MINDO/2 quantum chemical calculations of the changes of the potential energy along the reaction coordinates, have demonstrated that when one of the hydrogen atoms in ethylene is substituted by the methyl group, i.e. propylene is used instead of ethylene, a new reaction path leading to propylene peroxide appears, characterized by a much lower potential barrier than the reaction path to propylene oxide /Fig.9/. This is an elegant explanation of the observation that on silver catalysts propylene forms the total oxidation products whereas ethylene is oxidized selectively to ethylene oxide.

Results of our discussion are summarized in Fig.10. When oxygen is activated at the surface of the catalyst, ionic radical oxygen species O^- and O_2^- are formed which show very high activity in catalytic reactions and are the main oxidizing species in the total oxidation of simple molecules such as H_2 , CO, CH_4 etc. They may be considered as electrophilic reagents,

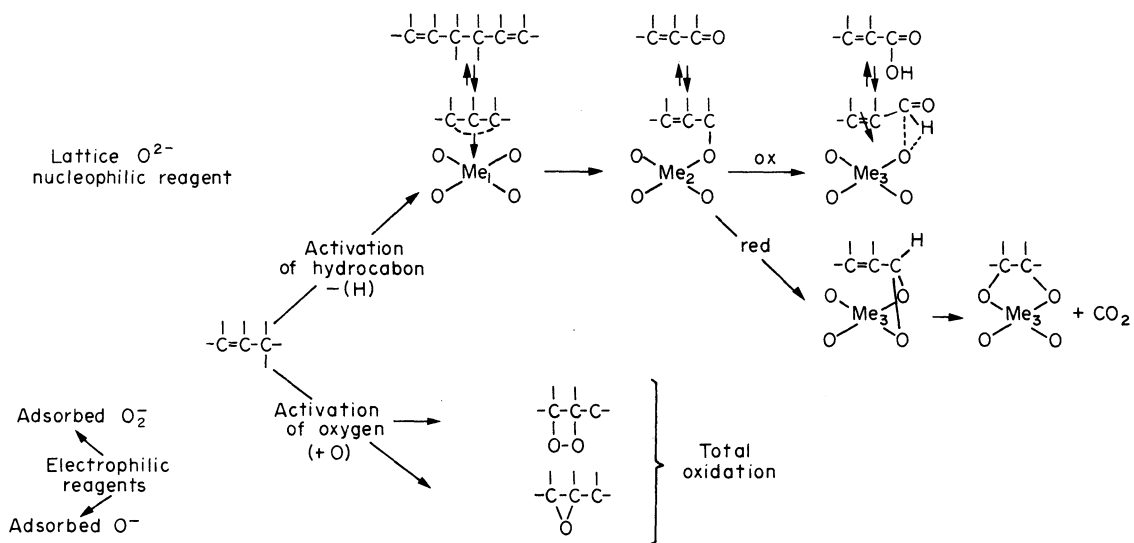


Fig.10. Mechanism of the oxidation of hydrocarbons.

which in reactions with olefins attack the molecule in the regions of highest electron density. Such electrophilic addition of O_2^- or O^- results in the formation of peroxy- or epoxy- complexes, respectively, which in the conditions of heterogeneous catalytic oxidation are intermediates of the degradation of the carbon skeleton and total oxidation.

When hydrocarbon molecule is activated, a different reaction path is initiated, consisting in the series of consecutive oxidative steps, each of them requiring different active centers to be present at the catalyst surface. The type of product obtained depends thus on the type and mutual proportions of these centers, as well as on the ratio of the rate of desorption of the particular intermediate complex to the rate of its transformation into the intermediate complex next in the series. This rate may strongly depend on the degree of reduction of the surface, attained in the course of the reaction, as it is the case with the carboxylate complex. On oxidized surface this complex desorbs in the form of acid, whereas on reduced surface it undergoes the decarboxylation, resulting in the deposition of coke. It should be emphasized that in the reaction path of partial oxidation it is the cations of the catalyst which act as oxidizing agents in one of the consecutive steps of the series, forming electrophilic hydrocarbon species. The lattice oxygen ions are nucleophilic reagents which have no oxidizing properties. They are inserted into the activated hydrocarbon molecule by nucleophilic addition, forming an oxygenated product, which after desorption leaves an oxygen vacancy at the surface of the catalyst. Such vacancies are then filled with oxygen from the gas phase, reoxidizing simultaneously the reduced cations.

REFERENCES

1. W.M.H. Saechtler, Catalysis Rev. **4**, 27 /1971/.
2. L.Ja. Margolis, Catalysis Rev. **8**, 241 /1974/.
3. C.R. Adams, H.H. Voge, Adv. Catal. **17**, 193 /1969/.
4. J. Haber, Z. Chem. **13**, 241 /1973/.
5. F. Vestch, J.L. Callahan, E.C. Milberger, R.W. Foreman, Proc. 2nd Intern. Congr. Catalysis, Paris 1960, **2**, 2647 /1961/.
6. J.L. Callahan, R.K. Grasselli, E.C. Milberger, H.A. Strecker, Ind. Eng. Chem., Prod. Res. Develop. **9**, 134 /1970/.
7. G.K. Boreskov, V.V. Popovskij, V.A. Sazonov, Proc. 4th Intern. Congr. Catalysis, Moscow 1968, **1**, 343 /1970/.
8. G.K. Boreskov, Kin. Kataliz, **14**, 7 /1973/.
9. G.N. Keulks, J. Catal. **19**, 232 /1970/.
10. C.R. Adams, Proc. 3rd Intern. Congr. Catalysis, Amsterdam 1964, **1**, 240 /1965/.
11. A. Bielański, M. Najbar, J. Catal. **25**, 398 /1972/.
12. J. Nowotny, J. Materials Sci. **12**, 1143 /1977/.
13. A. Bielański, J. Haber, Catal. Rev. /in print/.
14. Z. Dziewięcki, J. Haber, Mielczarska, React. Kin. Catal. Lett. **3**, 55 /1975/.
15. J. Haber, Mielczarska, unpublished results.
16. J. Haber, B. Grzybowska, J. Catal. **28**, 489 /1973/.

17. B. Grzybowska, K. German, J. Haber, T. Kowalski, A. Męzurkiewicz, Proc. Symp. Mechanism of Hydrocarbons Reactions, Siofok 1974, Akademiai Kiado, Budapest 1975, p. 265.
18. K. German, Ph.D. Thesis, Kraków 1973.
19. J. Haber, M. Sochacka, B. Grzybowska, A. Gołębiowski, J. Molecular Catal. **1**, 35 /1975/.
20. B. Grzybowska, J. Haber, J. Janas, J. Catal. **49**, 150 /1977/.
21. K. German, B. Grzybowska, J. Haber, Bull. Acad. Polon. Sci., ser. sci. chim. **21**, 319 /1973/.
22. T. Seijama, M. Egashira, T. Sakamoto, I. Aso, J. Catal. **24**, 76 /1972/.
23. T. Seiyama, N. Yanzoe, N. Egashira, Proc. 5th Intern. Congr. Catalysis, Palm Beach 1972, **2**, 997 /1973/.
24. G.I. Golodetz, Dokl. Akad. Nauk SSSR, **184**, 1334 /1969/.
25. M. Ai, 26th Intern. Congr. of Pure Appl. Chem., Tokyo 1977, Section Ia, paper 8F4-15.
26. M. Ai, T. Ikawa, J. Catal. **40**, 203 /1975/.
27. B. Grzybowska, M. Gašior, J. Catal. /in print/.
28. Y. Ohkatsu, M. Takeda, T. Hara, T. Osa, A. Misono, Bull. Chem. Soc. Japan **40**, 1413 /1967/; *ibid.* 2111.
29. R. Grabowski, J. Haber, J. Słoczyński, unpublished results.
30. J. Haber, M. Sochacka, A. Gołębiowski, J. Molecular Catal. **3**, 213 /1977/.
31. J. Haber, A. Kozłowska, Bull. Acad. Polon. Sci., ser. sci. chim. /in print/.
32. J. Haber, A. Kozłowska, J. Słoczyński, Bull. Acad. Polon. Sci., ser. sci. chim. **24**, 875 /1976/.
33. J. Haber, W. Marczewski, J. Stoch, L. Ungier, Proc. 6th Intern. Congr. Catalysis, London 1976, **2**, 827 /1977/.
34. J. Haber, J. Janas, Proc. Reunion Intern. Cinetique des Reactions dans les Systemés Chimique Heterogènes, Dijon 1974, Elsevier Amsterdam 1975, p. 737.
35. M. O'Keefe, in: "Fast ion transport in solids", North Holland Publ.Co., Amsterdam 1973, p. 233.
36. J. Haber, W. Marczewski, J. Stoch, L. Ungier, Ber. Bunsenges, phys. Chem. **79**, 970 /1975/.
37. J. Haber, J. Stoch, L. Ungier, J. Solid State Chem. **19**, 113 /1976/.
38. B. Grzybowska, J. Haber, W. Marczewski, L. Ungier, J. Catal. **42**, 327 /1976/.
39. P.A. Kilty, N.C. Rol. W.M.H. Sechtler, Proc. 5th Intern. Congr. Catalysis, Palm Beach 1972, **2**, 929 /1973/.
40. S. Beran, P. Jiru, B. Wichterlowa, R. Zehradnik, React. Kinet. Catal. Lett. **5**, 131 /1976/.